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X C D F O R

A FORTRAN IV PROGRAM FOR CALCULATING EQUILIBRIA

ON T-X_{CO₂} SECTIONS

BY

G.B. SKIPPEN AND W. YZERDRAAT

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I. General

The FORTRAN-IV program, XCDFOR, was written to calculate the position of mineral reaction curves on isobaric plots of the mole fraction of CO_2 in a CO_2 - H_2O fluid against temperature. Mixed volatile reactions as well as simple dehydration or decarbonation reactions can be located. A number of options are provided in the program and these are described in detail below. For most applications the options are not necessary and the program is used in a standard mode with the following input data cards:

1. A mandatory option card, this card to be left blank if no options are used.
2. A reaction definition card for each reaction to be calculated. The following information is required on each card:

Columns 2 through 39 inclusive: identification of the reaction
 41 through 48 : the constant, A
 49 through 56 : the constant, B
 57 through 64 : the constant, C

where A, B, C are constants in an equation of the form,

$$\log(f_{\text{CO}_2}^n \cdot f_{\text{H}_2\text{O}}^m) = \frac{A}{T} + B + \frac{C(P-2000)}{T}$$

Columns 65 through 70: The number of moles of CO_2 from the reaction stoichiometry (equivalent to the exponent n in the equilibrium equation). This number must be positive, i.e., the reaction must be written with CO_2 on the right-hand side. If CO_2 is not involved in the reaction, these columns are left blank.

Columns 71 through 76: The number of moles of H_2O from the reaction stoichiometry (equivalent to m in the equilibrium equation). It must be a positive number if both CO_2 and H_2O are involved on the same side of the reaction, or negative if CO_2 and H_2O are on opposite sides of the reaction. These columns are left blank if H_2O is not a component in the reaction.

Columns 77 through 80: Any positive number punched in these columns will result in a graphical display of the reaction curves.

Any number of reactions can be calculated by inserting a series of reaction definition cards. After the last such card, a data card with any negative number in columns 65 through 70 must be included to terminate the calculations.

The use of the above cards as data causes calculations to start at 730°C and proceed downwards at 5°C intervals until either the minimum temperature of 325°C is reached, or until no more useful results can be obtained. For each reaction, this series of calculations is first performed for a total gas pressure of 500 bars and then repeated for 1000 bars, 2000 bars, and 3000 bars.

Execution of the program requires approximately 8000 words of fast-memory (core) storage, a FORTRAN-IV compiler, a card reader, and a 130-position line printer.

For adaption to a 120-position line printer, only PRINT command 76, and print FORMATS 65 and 71 need to be modified, for example by removal of the redundant temperature column on the right side of the output.

II. Fugacity Coefficients

The method used in the program for determining equilibrium gas compositions is that described by Skippen (1971). The method requires fugacity coefficients for CO₂ and H₂O over the pressure and temperature range used in the program. At present, the required data are not available for CO₂-H₂O mixtures and it is necessary to use fugacity coefficients for the pure gases at the temperature and total pressure of the calculations. Fugacity coefficients tabulated by Burnham, Holloway and Davis (1969) for H₂O and tabulated for CO₂ by Skippen (1971) have been used. By curve-fitting techniques, a sixth degree power series was derived and the resulting fugacity coefficients derived from the built-in coefficients for H₂O fall within 0.1 to 0.5% of the values given by Burnham *et al.* The method used by Skippen (1971) to derive fugacity coefficients for CO₂ is subject to considerable uncertainty and little accuracy can be claimed for the primary data. The "reconstituted" coefficients from the program are in close agreement with the original values and wherever there is a noticeable difference, the computer-generated coefficients line up into a smoother curve than the original data. A listing of fugacity coefficients is possible through the option card, as described below.

In anticipation of better fugacity coefficient data from P-V-T measurements of CO₂-H₂O mixtures, two options have been provided for in the input data. Under input option 1, the user may substitute his own coefficients for a polynomial expression to fit the fugacity coefficient data. Under the second input option, the user may specify a list of fugacity coefficients without the necessity of fitting a polynomial expression to the fugacity coefficient data.

III. Input

The input data supplied by the user consist of

1. An option card . (mandatory)

2. A pressure specification card. (optional)
To be used if pressures other than the standard series of 500, 1000, 2000, and 3000 bars are used.
3. Fugacity coefficient deck. (optional)
If the user wishes, he may substitute for the built-in fugacity coefficients, either a deck containing coefficients for a polynomial expression or a deck of fugacity coefficients.
4. A set of reaction definition cards. (mandatory)
5. A termination card. (mandatory)
A negative number should be punched in the field defined by columns 65 through 70 of the termination card.

1. The option card

The program may be run in the standard mode by leaving the option card blank. Overall plotting of the output may be achieved by punching the numeral 1 in column 56 of the option card.

The standard mode provides the following:

- a) Automatic generation of a table of fugacity coefficients for H₂O and CO₂ at the four standard pressures in the temperature interval, 325° C-730° C. The table is not printed out unless called for under option 8 below.
- b) Calculation of equilibrium gas ratios for the standard pressures, 500, 1000, 2000 and 3000 bars, over the applicable part of the standard temperature interval, 325° C-730° C.
- c) Organization of the printed output in such a way that it is suitable for a vertical format of 42 lines per sheet.

The option card allows the following modifications:

1. Column 8
Blank or 0 for default.
Punch 1 for input option 1 (alternative set of polynomial coefficients for fugacity coefficient data).
Punch 2 for input option 2 (alternative set of fugacity coefficients punched directly on cards).
2. Column 16
Degree of power series for polynomial expression under input option 1.
3. Columns 21-24
Redefinition of upper temperature limit.

- | | |
|------------------|--|
| 4. Columns 29-32 | Redefinition of lower temperature limit. |
| 5. Column 40 | Modification of the standard series of pressures. Indicate the number of pressures to be calculated by punching 1 to 4. |
| 6. Columns 47-48 | Modification of standard temperature interval (i.e. std. value of 5°C). Indicate the desired interval by punching 1 to 20. |
| 7. Column 56 | Punch any number for overall plotting. |
| 8. Columns 61-64 | Punch any number for listing of fugacity coefficients. |
| 9. Columns 71-72 | Punch the number of lines per output page. |

1.1. Input options

There are three input options: 0, 1, and 2. Input option 0 is part of the standard mode; to implement it, nothing need be punched in column 8 of the option card. In this option, the program provides its own fugacity coefficients.

Input option 1

The user may substitute his own equation coefficients for the calculation of fugacity coefficients by first punching the numeral 1 in column 8 of the option card, and then presenting his own set of coefficients for a polynomial fit to fugacity coefficients immediately following the pressure definition card, or, if no pressure definition card is present, after the option card.

The equation in which these coefficients will be used to derive fugacity coefficients, is built into the program. It is a power series of potentially nine terms, that is, a series of the degree 8. However, unless the user specifies otherwise by punching the numeral representing the degree in column 16 of the option card, the standard assumption is that the degree should be 6, and consequently the program will attempt to read 7 coefficients for each gas species and for each pressure specified or assumed by default.

A detailed description of the set of polynomial coefficient cards is given later in the section on user-supplied coefficients.

Input option 2

In case the user wants to provide his own fugacity coefficients directly, he must first punch the numeral 2 in column 8 of the option card, and then present a deck of cards containing the necessary fugacity coefficients for the two gas species at the specified pressures.

A detailed description of this deck is given under the heading 'User-specified Coefficients'.

1.2. Specifying the degree of the equation called upon to calculate fugacity coefficients.

Column 16 of the option card may be used to specify the degree of the power-series from which the fugacity coefficients will be derived after the user has supplied his own equation coefficients. Consequently, this option is only applicable under input option 1. Under the other input options, column 16 of the option card will be ignored.

The lowest permissible degree is 3, the highest 8. Illegal values are automatically replaced: by 6 if specified too low, by 8 if too high.

1.3. Specifying the upper temperature limit.

Columns 21-24 of the option card represent an I4-field to specify an alternative maximum temperature (right-justified). The default value is 730°C; this is the maximum of the range within which the built-in fugacity coefficients apply. User-specified maxima above this temperature will automatically be reduced to 730°C unless the user first modifies the safe-guard-statement XCDFR 25: MAXPRO = 730.

1.4. Specifying the lower temperature limit

The I4-field defined by columns 29-32 of the option card is available for re-definition of the minimum temperature. The default value of 325°C is the program minimum below which the program-generated fugacity coefficients do not apply. Statement XCDFR 26, MINPRO = 325, safeguards against minima which are specified too low through the option under discussion; therefore, if the user wants to have calculations done for temperatures below 325°C, he must first modify this statement and supply his own coefficients.

The following restrictions should be borne in mind:

1. The program will automatically re-adjust the minimum temperature if it is more than 405° lower than the maximum temperature.
2. Automatic adjustment will ensue if the minimum temperature is less than 80° lower than the maximum temperature.
3. The same will happen if the range between minimum and maximum is less than 20 times the specified interval, or if it is greater than 81 times the specified interval.

In all these cases it is only the minimum temperature that is reset. In most cases, therefore, where statement XCDFR 26 is modified, the preceding statement should also be adjusted.

1.5. Specifying alternative pressures

Column 40 of the option card may be used to modify the standard series of four pressures (500, 1000, 2000, 3000 bars), or to specify a smaller number of pressures for which calculations are to be done.

The desired number of different pressures should be punched in column 40; the minimum is 1, the maximum 4. Illegal values are replaced by the default value 4.

Any numerical punch in column 40, other than 0, renders use of a pressure specification card mandatory. This card is described below.

1.6. Modifying the standard temperature interval

Column 48 (or columns 47-48) of the option card may be used to specify the temperature interval for the calculation of successive equilibrium gas ratios. The program accepts any value from 1 to 20; if a higher integer is punched, the value will be reset to 20°C. The default value is 5°C.

1.7. Calling for overall plotting

Column 56 controls the overall plotting facility. Any numeral punched in this column or in one of the three preceding columns will result in the production of line-printer diagrams for every reaction, regardless of any positive or negative values which may appear in the last field of the reaction-definition cards.

1.8. Calling for coefficient listing(s)

Any numeral punched in column 64 or in one of the three preceding columns of the option card will produce, under any input option, a listing of the relevant fugacity coefficients. Under input options 0 and 1, this listing is preceded by a listing of the equation coefficients.

1.9. Changing the vertical output format

Columns 71-72 of the option card may be used to specify a number of lines per output page other than the standard number of 42. Where 11-inch high printer forms are in use, the appearance of the diagrams can be improved by specifying 60 to 62 lines per page through this option.

2. The pressure specification card

This card becomes mandatory where any numeral other than 0 has been punched in column 40 of the option card. It is compatible with the use of input option 0 provided the pressures specified in it are identical with the pressures forming the first part of the standard series and appear in the same order. In all other cases, input option 1 or input option 2 must be used to adjust fugacity coefficient data to the new pressure(s).

The format of the pressure specification card is (4(4X, I4)) and consequently the first-specified pressure must be punched right-justified in the field defined by columns 5-8, and so on.

If the program is run under either input option 1 or 2, the user-supplied coefficients must be presented in an arrangement corresponding to the order in which the pressures are given in the pressure-specification card.

3. User-supplied coefficients

If the user has chosen input option 1, he must now provide polynomial coefficients to replace those from which the program would normally have derived the fugacity coefficients.

Under input option 2, the user may not replace the built-in polynomial coefficients; the program will look directly for user-supplied fugacity coefficients, and ignore the polynomial coefficients.

Both types of coefficients must be presented as a set of cards immediately following the pressure specification card, or, if the latter is not present, immediately following the option card.

Polynomial coefficients

One set of polynomial coefficients is needed for each pressure and for each gas species; this implies that the number of sets of coefficients is twice the number of pressures. All the coefficients pertaining to H₂O fugacity calculations must be given before those for carbon dioxide can be given. The very first set of equation coefficients must, therefore, refer to the fugacity calculations for water at the first-specified (or lowest standard) pressure; the second set must refer to the fugacity calculations for water at the second-specified (or second-lowest standard) pressure, and so on.

Each individual set of equation coefficients must be arranged in order of ascending powers of the terms of the power series. The computer will attempt to read one more coefficient than the number indicated by the degree of the power series.

As the reading format of the coefficient cards is (5(1X, E14.8)), the last digit of each E-field should be in one of the columns 15, 30, 45, 60, or 75 of the card. Certain compilers impose more stringent requirements in this respect than others.

Each card, under the above format, may contain up to five coefficients. Therefore, specification of a degree higher than 4 will require the use of card pairs. This is probably the most common case; therefore, normally, the number of cards in the entire polynomial coefficient deck will equal four times the number of pressures.

If the number of terms in the power series is not the same for each gas species at every required pressure, the user should specify the highest degree required in any of the equations. If this degree is 6, he need not take any action in this respect; otherwise, he must punch a numeral in column 16 of the option card. Furthermore, if a card pair is needed for the equation coefficients of this highest degree, then card pairs must be presented throughout, even though any or all second cards of the other pairs may have to be left blank. All defaulted coefficients will be interpreted as having the value 0, and thus will not affect the outcome of the calculation of fugacity coefficients.

Fugacity coefficients

Under input option 2, the fugacity coefficients must be read in directly. Coefficients must be given for the maximum temperature as well as for the minimum temperature; the user can provide as many values for intervening integer Centigrade temperatures as he thinks useful for his purpose. The program will perform linear interpolation to derive coefficients at intervals of 1°C. There is no provision for extrapolation; therefore, the user must make sure that his deck contains cards for the minimum as well as for the maximum temperature. If these fugacity coefficients are missing, the program will attempt to reset minimum and/or maximum temperature until the above-mentioned condition is satisfied for each gas species at every specified pressure. Should this effort fail, then the program will print a diagnostic message and proceed to run the reaction input with its own coefficients.

The fugacity coefficient cards need not be presented in any particular order. For any given temperature, the last-read coefficients will overwrite any prior values. Thus it is possible to rectify faulty coefficients, after detection, by simply adding a card with corrected coefficients at the end of the deck.

The very last card of this deck must be left blank. Not more than 999 cards can be read in. The 999th card, if present, does not have to be a blank card.

Each card must contain the temperature to which it refers, punched as a right-justified integer in the field defined by columns 5-8. The next value in this card, punched in the F8-field immediately following the temperature field, will be understood to represent the fugacity coefficient for water at the first-specified (or lowest standard) pressure; the following value will be understood to represent the fugacity coefficient of water at the second-specified pressure, or, if only one pressure is specified, as the fugacity coefficient of carbon dioxide at that pressure.

After all (1 to 4) coefficients for water have been given, the next value is understood to be the first coefficient of CO_2 . Thus, if there is only one pressure, the effective format of the card is (4X, I4, 2F8.4), although it is specified in the program as (4X, I4, 8F8.4).

4. Reaction definition cards

Depending upon the combination of options chosen, the first reaction definition card follows either the option card, or the pressure specification card, or the set of equation coefficient cards, or the card terminating the deck of fugacity coefficient cards. This effectively means that, aside from the termination card, the reaction definition cards form the last section of the user-supplied input. There is no limit to their number.

Of each reaction definition card, the first half is available for identification of the reaction. This information is used exclusively in page headings and diagram headings. It is recommended that the first and the 40th column be left blank. The remaining information to be punched on these cards has been previously described, beginning on page 3.

5. The termination card

This card should contain a negative number in the field defined by columns 65 through 70. This will notify the program that no more reaction definition cards are to be read and that the routine "EXIT" should be called.

IV. Output

The output of XCDFOR is entirely in the form of print. Standard line width is 130 real printing positions. Only two format specifications,

however, require a width of more than 120 columns - see section I.

There are five types of output:

1. A listing of coefficients for a polynomial expression for fugacity coefficients (optional, called by punching a numeral in column 64 of the option card).
2. A listing of fugacity coefficients over the chosen temperature range (at 1° intervals, in descending order) for both H_2O and CO_2 for each of the maximum four pressures chosen or accepted by default. This listing is optional (it, too, is called by punching a numeral in column 64 of the option card).
3. Tables of equilibrium gas composition data, listing maximum temperatures, if within the program temperature range, mole fractions CO_2 , and pressures and fugacities for the gas species involved in the reaction.
4. Diagrams representing the equilibrium curves for all pressures represented by the tabulated output just described (diagrams optional, called by either a numerical punch in column 56 of the option card, or a numerical punch in column 80 of the reaction specification card, or both).
5. Two types of diagnostic output: the first to warn the user that an omission or error was found in his deck of fugacity coefficients (under input option 2); the second type to indicate that no suitable values of equilibrium compositions could be derived from the data provided. The latter case may happen where the maximum temperature of an equilibrium curve is found to be beneath the minimum temperature the program is required to handle; in such cases, no diagram, of course, can be shown either. There may also be cases where printed values can be tabulated, but no diagram can be shown because the values in question would, after rounding, coincide with the vertical boundaries of the diagram.

It is appropriate here to mention the two rescue routines which may take temporary control of program execution after printing a diagnostic message of the first kind. Where the error is serious enough to preclude usage of the user-supplied fugacity coefficients altogether, the program will attempt to process the reaction data with the help of its own "reconstituted" fugacity coefficients. Where minor errors are found in this input deck, the program will utilize the usable portion of the fugacity coefficients and adapt its minimum and maximum temperature accordingly.

V. The plot

The plotting subroutine can be called by punching a numeral in column 56 of the option card, or, if desired for certain reactions only, by punching a numeral in column 80 of the reaction definition cards. If the latter method is chosen, the plotting facility can later be suppressed again by rendering that number negative.

In the diagram itself, a one-line caption identifies the reaction in the terms stated by the user in the first 40 columns of the reaction definition card, and adds the values of the pressure(s) for which equilibrium curves are shown.

In the diagram, points on the curve representing the lowest pressure are shown as dots; those on the curve for the next-higher pressure are shown as plus-signs; those on the next curve as asterisks, and those on the curve for the highest pressure as zeros. This technique allows representation of all four (or fewer) curves in one figure.

The positions of the points shown are defined by (vertically) the temperature for which the composition of the gas species has been determined, and (horizontally) the mole fraction of CO_2 in the gas phase. Along the vertical axes, temperatures are indicated at intervals five times the standard program interval (or five times the user-defined interval). If a curve maximum does not coincide with a multiple of the standard interval, the temperature of this maximum will be shown in the margin on the line which would be occupied by the next-higher multiple of the standard interval. This procedure may occasionally give rise to slight distortion of the plotted curve. The appearance of the odd temperature in the plot margin should draw the user's attention to the cause of this apparent distortion.

Whereas the vertical control of the curve points is based on temperature values which are always integers, horizontal control depends on equilibrium ratios which must first be rounded to the nearest multiple of 0.01. This permits only representation of those values which lie between 0.005 and 0.995; any equilibrium ratio outside this range would cause the curve point to coincide with one of the vertical boundaries of the plot. Tests in the plotting routine will prevent this from happening, unless the value in question represents the maximum of a reaction involving one gas species only.

If more curve points must be shown than can be accommodated on one page, the plotting routine will first determine whether it is necessary to print yet another page; this is deemed to be the case if there is at least one point left to be shown within the equilibrium composition range between 0.1 and 0.9. In such a case, printing on the next page will be resumed at such a temperature level that the sheet will be filled out as completely as possible; almost invariably this will entail a certain overlap of the two parts of the diagram. In no case will there be an omission of significant equilibrium points.

If further diagram printing on a fresh page is found to be unnecessary, the figure is completed by a horizontal line with a scale division in tenths to indicate the mole fraction of CO_2 represented by the horizontal direction in the graph.

References Cited

- Burnham, C.W., Holloway, J.R., Davis, N.F. 1969. Thermodynamic properties of water to 1000°C and 10,000 bars. Geol. Soc. Am. Special Paper 132, 96 pp.

Skippen, G.B. 1971. Experimental data for reactions in siliceous marbles. *Jour. Geol.*, 79, pp. 457-481.


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DIMENSION FC(8),TEMPER(8),TEMP(406,8),FUCOEF(406,8) XCDFOR 1
COMMON FUCOEF XCDFOR 2
COMMON/AAA/EQCOEF(2,4,9),WORD(3) XCDFOR 3
COMMON/BBB/IPRES(4),RENAME(10),SYMBLL(10),PLINE(101),IRA(83,4,3) XCDFOR 4
EQUIVALENCE (TEMP,FUCOEF) XCDFOR 5
C *** EXTERNAL ECONF (ONLY FOR SUS AND IBM COMPILERS) XCDFOR 6
ECONF(TEMPK)=10.** (A/TEMPK+B) XCDFOR 7

CALL EOFSET(1065)
DATA SYMBOL/ 1H., 1H+, 1H*, 1H0, 1H , 1HI, 1H-, 1H-, 1H XCDFOR 9
DATA WORD/ 4H H2O, 4H CO2, 4H PAR/ XCDFOR 10
DATA IPRES/ 500, 1000, 2000, 3000/ XCDFOR 11
DATA EQCOEF/6.017635,-.25121724,-1.2042135,-.50722465,-.56129643, XCDFOR 12
1 2.105797,-.57907187,1.7840157,-.063509832,.0078615211,.018139648, XCDFOR 13
2 .010330951,.0083421085,-.0047083335,.0086120867,.0086443766, XCDFOR 14
3 .00025322866,-.16655348E-4,-.00011004716,-.22026544E-4, XCDFOR 15
4 -.50544549E-4,.16964035E-4,-.52198619E-4,-.24657175E-4, XCDFOR 16
5 -.46545618E-6,.16018889E-7,.34139617E-6,.21382778E-7,.15822439E-6, XCDFOR 17
6 -.22837663E-7,.16420945E-6,.2885E-7,.410891E-9,-.58333333E-11, XCDFOR 18
7 -.54188497E-9,-.79166667E-11,-.24822086E-9,.10416667E-10, XCDFOR 19
8 -.2612E-9,-.125E-10,-.14150667E-12,0,.42941572E-12,0, XCDFOR 20
9 .19459203E-12,0,.20869719E-12,0,0,0,-.13577122E-15,0, XCDFOR 21
* -.61359392E-16,0,-.67096305E-16,17#0/ XCDFOR 22
C *** XCDFOR 23
C * SAFEGUARDS AND DEFAULT FACILITIES ARE BUILT IN HERE XCDFOR 24
C *** XCDFOR 25
MAXPRO=730 XCDFOR 26
MINPRO=325 XCDFOR 27
IF (MINPRO.LT.MAXPRO-405) MINPRO=MAXPRO-405 XCDFOR 28
1 READ 1,INPOPT,NDGREE,MAXTEM,MINTEM,NOPRES,INTVAL,IPL0T,NOC0EF,LP XCDFOR 29
FORMAT(10(4X,14)) XCDFOR 30
IF (INTVAL.GT.20) INTVAL=20 XCDFOR 31
IF (INPOPT.LT.0) INPOPT=IABS(INPOPT) XCDFOR 32
IF (INPOPT.GT.2) INPOPT=2 XCDFOR 33
IF (LP.EQ.0) LP=42 XCDFOR 34
IF (NOPRES.EQ.0) GO TO 201 XCDFOR 35
READ 1,(IPRES(J),J=1,NOPRES) XCDFOR 36
201 IF (INTVAL.LE.0) INTVAL=5 XCDFOR 37
MRANGE=INTVAL*81 XCDFOR 38
IF (MINPRO.LT.MAXPRO-MRANGE) MINPRO=MAXPRO-MRANGE XCDFOR 39
MRANGE=20*INTVAL XCDFOR 40
IF (MINPRO.GT.MAXPRO-MRANGE) MINPRO=MAXPRO-MRANGE XCDFOR 41
IF (MAXPRO-MINPRO.GT.405) MINPRO=MAXPRO-405 XCDFOR 42
IF (NDGREE.LT.3) NDGREE=6 XCDFOR 43
IF (NDGREE.GT.8) NDGREE=8 XCDFOR 44
IF (INPOPT.EQ.0) NDGREE=6 XCDFOR 45
IF (MAXTEM.LT.MINPRO) MAXTEM=MAXPRO XCDFOR 46
IF (MAXTEM.LT.MINPRO+80) MAXTEM=MINPRO+80 XCDFOR 47
IF (MAXTEM.GT.MAXPRO) MAXTEM=MAXPRO XCDFOR 48
IF (MINTEM.LT.MINPRO) MINTEM=MINPRO XCDFOR 49
IF (MAXTEM-MINTEM.LT.80) MINTEM=MAXTEM-80 XCDFOR 50
IF (NOPRES.LT.1) NOPRES=4 XCDFOR 51
IF (NOPRES.GT.4) NOPRES=4 XCDFOR 52
NP=NOPRES+NOPRES XCDFOR 53
LDGREE=NDGREE+1 XCDFOR 54
MSTART=MAXTEM+1 XCDFOR 55
KELMIN=MINTEM+273 XCDFOR 56
BOTTEM=KELMIN XCDFOR 57
IGRADE=MSTART-MINTEM XCDFOR 58
ITEST=MAXTEM/INTVAL XCDFOR 59
ITEST=ITEST*INTVAL XCDFOR 60
IF (ITEST.EQ.MAXTEM) GO TO 202 XCDFOR 61
ITEST=ITEST+INTVAL XCDFOR 62
202 IP=ITEST+INTVAL XCDFOR 63
IF (INPOPT-1) 17,17,2 XCDFOR 64
C *** XCDFOR 65
COEFFICIENTS READ IN UNDER INPUT OPTION 2 ARE HANDLED IN THIS SEGMENT XCDFOR 66
C *** XCDFOR 67
2 DO 3 I=1,IGRADE XCDFOR 68
DO 3 J=1,NP XCDFOR 69
FUCOEF(I,J)=0 XCDFOR 70
3 CONTINUE XCDFOR 71
DO 6 I=1,999 XCDFOR 72
READ 4,IT,(FC(J),J=1,NP) XCDFOR 73
4 FORMAT(4X,14,8F8.4) XCDFOR 74
IF (IT.GT.MAXTEM) GO TO 6 XCDFOR 75
IF (IT.EQ.0) GO TO 7 XCDFOR 76
IF (IT.LT.MINTEM) GO TO 6 XCDFOR 77
IT=MSTART-IT XCDFOR 78
DO 5 J=1,NP XCDFOR 79
FUCOEF(IT,J)=FC(J) XCDFOR 80
5 CONTINUE XCDFOR 81
6 CONTINUE XCDFOR 82
7 INDEX=0 XCDFOR 83
C *** XCDFOR 84
CHECK-LOOP VERIFIES PRESENCE OF FUGACITY COEFFICIENTS AT MINIMUM AND XCDFOR 85
C * MAXIMUM TEMPERATURES SPECIFIED OF PROGRAM-DETERMINED XCDFOR 86
C *** XCDFOR 87
DO 14 I=1,NP XCDFOR 87

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ITO=MSTART-MINTEM	XCDFR 88
IF(FUCOEF(ITO,I).LE.0) GO TO 140	XCDFR 89
ITO=1	XCDFR 90
IF(FUCOEF(ITO,I).LE.0) GO TO 142	XCDFR 91
MIS=0	XCDFR 92
ITOP=1	XCDFR 93
C ***	XCDFR 94
C * START OF INTERPOLATION UNDER INPUT OPTION 2	XCDFR 95
C ***	XCDFR 96
DO 13 I=1,IGRADE	XCDFR 97
IF(FUCOEF(IT,I).LE.0.) GO TO 9	XCDFR 98
IF(MIS.GT.0) GO TO 10	XCDFR 99
COEF=FUCOEF(IT,I)	XCDF 100
GO TO 12	XCDF 101
9 MIS=MIS+1	XCDF 102
GO TO 13	XCDF 103
10 STEPS=MIS+1	XCDF 104
STEPS=(FUCOEF(IT,I)-COEF)/STEPS	XCDF 105
COEF=FUCOEF(IT,I)	XCDF 106
K=ITOP	XCDF 107
DO 11 J=1,MIS	XCDF 108
L=K	XCDF 109
K=K+1	XCDF 110
FUCOEF(K,I)=FUCOEF(L,I)+STEPS	XCDF 111
11 CONTINUE	XCDF 112
MIS=0	XCDF 113
12 ITOP=IT	XCDF 114
13 CONTINUE	XCDF 115
14 CONTINUE	XCDF 116
IF(NOCOEF)520,520,500	XCDF 117
C ***	XCDF 118
C * THE FOLLOWING STATEMENTS EMBODY RESCUE ROUTINES TO ENSURE SUCCESS-	XCDF 119
C * FUL EXECUTION EVEN IF USER FAILED TO PROVIDE FUGACITY COEFFICIENTS.	XCDF 120
C * AT THE EXACT MAXIMUM AND MINIMUM TEMPERATURES SPECIFIED OR PROVIDED	XCDF 121
C ***	XCDF 122
140 ITO=ITO-1	XCDF 123
MINTEM=MINTEM+1	XCDF 124
IF(MAXTEM-MINTEM.LT.80) GO TO 15	XCDF 125
IF(FUCOEF(ITO,I).LE.0) GO TO 140	XCDF 126
KELMIN=MINTEM+273	XCDF 127
BOTTEM=KELMIN	XCDF 128
IGRADE=MSTART-MINTEM	XCDF 129
GO TO 7	XCDF 130
142 INDEX=INDEX+1	XCDF 131
MAXTEM=MAXTEM-1	XCDF 132
IF(MAXTEM-MINTEM.LT.80) GO TO 15	XCDF 133
ITO=ITO+1	XCDF 134
IF(FUCOEF(ITO,I).LE.0) GO TO 142	XCDF 135
MSTART=MAXTEM+1	XCDF 136
IGRADE=MSTART-MINTEM	XCDF 137
ITEST=MAXTEM/INTVAL	XCDF 138
ITEST1=ITEST*INTVAL	XCDF 139
IF(ITEST.EQ.MAXTEM) GO TO 141	XCDF 140
ITEST=ITEST1+INTVAL	XCDF 141
141 IP=ITEST+INTVAL	XCDF 142
DO 143 I=1,IGRADE	XCDF 143
K=I+INDEX	XCDF 144
DO 143 J=1,NP	XCDF 145
FUCOEF(I,J)=FUCOEF(K,J)	XCDF 146
143 CONTINUE	XCDF 147
GO TO 7	XCDF 148
15 PRINT 16	XCDF 149
16 FORMAT(49H SORRY, CANNOT FIND YOUR FUGACITY COEFFICIENTS.	XCDF 150
1 49H WILL NOW RUN YOUR DATA WITH MY OWB COEFFICIENTS. /)	XCDF 151
INOPT=0	XCDF 152
NDGREE=6	XCDF 153
MAXPRO=730	XCDF 154
MINPRO=325	XCDF 155
MAXTEM=0	XCDF 156
MINTEM=0	XCDF 157
INTVAL=5	XCDF 158
IPLOT=1	XCDF 159
NOCOEF=1	XCDF 160
GO TO 201	XCDF 161
C ***	XCDF 162
C * END OF RESCUE ROUTINES, START OF CALCULATION OF FUGACITY	XCDF 163
COEFFICIENTS UNDER INPUT OPTION 0 UR 1	XCDF 164
C ***	XCDF 165
17 T=MSTART	XCDF 166
DO 18 N=1,IGRADE	XCDF 167
T=T-1.	XCDF 168
TEMP(N,1)=T	XCDF 169
DO 18 M=2,NDGREE	XCDF 170
L=M-1	XCDF 171
TEMP(N,M)=TEMP(N,L)*T	XCDF 172
18 CONTINUE	XCDF 173
IF(NOCOEF.EQ.0) GO TO 231	XCDF 174
PRINT 23	XCDF 175

23	FORMAT(1H1,30X,45HEQUATION COEFFICIENTS USED IN CALCULATION OF	XCDF 176
	1 21HFUGACITY COEFFICIENTS,/))	XCDF 177
231	DO 29 N=1,2	XCDF 178
	DO 27 M=1,NOPRES	XCDF 179
	IF(INPOP1.NE.1) GO TO 25	XCDF 180
	READ 24,(EQCOEF(N,M,L),L=1,LDGREE)	XCDF 181
24	FORMAT(5(1X,E14.8)/4(1X,E14.8))	XCDF 182
25	IF(NOCDEF.EQ.0) GO TO 27	XCDF 183
	PRINT 26,WORD(N),IPRES(M),WORD(3),(EQCOEF(N,M,L),L=1,LDGREE)	XCDF 184
26	FORMAT(1H0,A4,I5,A4,7(2X,E14.8)/14X,2(2X,E14.8)/)	XCDF 185
27	CONTINUE	XCDF 186
	IF(NOCDEF.EQ.0) GO TO 29	XCDF 187
	PRINT 28	XCDF 188
28	FORMAT(1H0,/))	XCDF 189
29	CONTINUE	XCDF 190
	LINES=LP	XCDF 191
	DO 52 IT=1,IGRADE	XCDF 192
	DO 30 I=1,NDGREE	XCDF 193
	TEMPER(I)=TEMP(IT,I)	XCDF 194
30	CONTINUE	XCDF 195
	DO 32 N=1,NOPRES	XCDF 196
	NG=N	XCDF 197
	DO 32 I=1,2	XCDF 198
	FUCOEF(IT,NG)=EQCOEF(I,N,1)	XCDF 199
	DO 31 L=2,LDGREE	XCDF 200
	K=L-1	XCDF 201
	FUCOEF(IT,NG)=FUCOEF(IT,NG)+EQCOEF(I,N,L)*TEMPER(K)	XCDF 202
31	CONTINUE	XCDF 203
	NG=NG+NOPRES	XCDF 204
32	CONTINUE	XCDF 205
	IF(NOCDEF.EQ.0) GO TO 52	XCDF 206
	IF(LINES.LT.LP) GO TO 42	XCDF 207
	GO TO (320,322,324,326),NOPRES	XCDF 208
320	PRINT 321,IPRES(1),WORD(3)	XCDF 209
321	FORMAT(25HFUGACITY COEFFICIENTS AT,I5,A4)	XCDF 210
	GO TO 328	XCDF 211
322	PRINT 323,IPRES(1),IPRES(2),WORD(3)	XCDF 212
323	FORMAT(1H1,2X,24HFUGACITY COEFFICIENTS AT,I5,4H AND,I5,A4)	XCDF 213
	GO TO 328	XCDF 214
324	PRINT 325,(IPRES(J),J=1,3),WORD(3)	XCDF 215
325	FORMAT(1H1,7X,38HFUGACITY COEFFICIENTS AT THE PRESSURES,	XCDF 216
	1 2(I5,1H,),4H AND,I5,A4)	XCDF 217
	GO TO 328	XCDF 218
326	PRINT 327,(IPRES(J),J=1,4),WORD(3)	XCDF 219
327	FORMAT(1H1,12X,38HFUGACITY COEFFICIENTS AT THE PRESSURES,	XCDF 220
	1 2(I5,1H,),4H AND,I5,A4)	XCDF 221
328	GO TO (33,35,37,39),NOPRES	XCDF 222
33	PRINT 34	XCDF 223
34	FORMAT(1H0,12X,5HWATER,6X,14HCARBON DIOXIDE,/,6H TEMP,/-	XCDF 224
	GO TO 41	XCDF 225
35	PRINT 36	XCDF 226
36	FORMAT(1H0,17X,5HWATER,10X,14HCARBON DIOXIDE,/,6H TEMP,	XCDF 227
	1 47X,4HTEMP,/))	XCDF 228
	GO TO 41	XCDF 228
37	PRINT 38	XCDF 229
38	FORMAT(1H0,19X,5HWATER,30X,14HCARBON DIOXIDE/6H TEMP,	XCDF 230
	1 33X,4HTEMP,37X,4HTEMP/))	XCDF 231
	GO TO 41	XCDF 232
39	PRINT 40	XCDF 233
40	FORMAT(1H0,23X,5HWATER,37X,14HCARBON DIOXIDE/6H TEMP,40X,	XCDF 234
	1 4HTEMP,44X,4HTEMP/))	XCDF 235
41	LINES=6	XCDF 236
42	ITEMP=TEMPER(1)	XCDF 237
	GO TO (43,45,47,49),NOPRES	XCDF 238
43	PRINT 44,ITEMP,(FUCOEF(IT,NG),NG=1,2)	XCDF 239
44	FORMAT(16,4X,F8.4,8X,F8.4)	XCDF 240
	GO TO 51	XCDF 241
45	PRINT 46,ITEMP,(FUCOEF(IT,NG),NG=1,4),ITEMP	XCDF 242
46	FORMAT(16,4X,2F8.4,3X,2F9.4,3X,I6)	XCDF 243
	GO TO 51	XCDF 244
47	PRINT 48,ITEMP,(FUCOEF(IT,NG),NG=1,3),ITEMP,(FUCOEF(IT,NG),NG=4,6)	XCDF 245
	1,ITEMP	XCDF 246
48	FORMAT(16,3X,3F8.4,3X,I6,3X,3F9.4,3X,I6)	XCDF 247
	GO TO 51	XCDF 248
49	PRINT 50,ITEMP,(FUCOEF(IT,NG),NG=1,4),ITEMP,(FUCOEF(IT,NG),NG=5,8)	XCDF 249
	1,ITEMP	XCDF 250
50	FORMAT(16,3X,4F8.4,3X,I6,3X,4F9.4,3X,I6)	XCDF 251
51	LINES=LINES+1	XCDF 252
52	CONTINUE	XCDF 253
	GO TO 520	XCDF 254
500	LINES=LP	XCDF 255
	ITEMP=MSTART	XCDF 256
	DO 512 IT=1,IGRADE	XCDF 257
	ITEMP=ITEMP-1	XCDF 258
	IF(LINES.LT.LP) GO TO 506	XCDF 259
	GO TO (520,532,534,536),NOPRES	XCDF 260
520	PRINT 321,IPRES(1),WORD(3)	XCDF 261
	GO TO 538	XCDF 262

532 PRINT 323,IPRES(1),IPRES(2),WORD(3)	XCDF 263
GO TO 53F	XCDF 264
534 PRINT 325,(IPRES(J),J=1,3),WORD(3)	XCDF 265
GO TO 538	XCDF 266
536 PRINT 327,(IPRES(J),J=1,4),WORD(3)	XCDF 267
538 GO TO (501,502,503,504),NOPRES	XCDF 268
501 PRINT 34	XCDF 269
GO TO 505	XCDF 270
502 PRINT 36	XCDF 271
GO TO 505	XCDF 272
503 PRINT 38	XCDF 273
GO TO 505	XCDF 274
504 PRINT 40	XCDF 275
505 LINES=6	XCDF 276
506 GO TO (507,506,509,510),NOPRES	XCDF 277
507 PRINT 44,ITEMP,(FUCDEF(IT,NG),NG=1,2)	XCDF 278
GO TO 511	XCDF 279
508 PRINT 46,ITEMP,(FUCDEF(IT,NG),NG=1,4),ITEMP	XCDF 280
GO TO 511	XCDF 281
509 PRINT 48,ITEMP,(FUCDEF(IT,NG),NG=1,3),ITEMP,(FUCDEF(IT,NG),NG=4,6)	XCDF 282
1,ITEMP	XCDF 283
GO TO 511	XCDF 284
510 PRINT 50,ITEMP,(FUCDEF(IT,NG),NG=1,4),ITEMP,(FUCDEF(IT,NG),NG=5,8)	XCDF 285
1,ITEMP	XCDF 286
511 LINES=LINES+1	XCDF 287
512 CONTINUE	XCDF 288
C ***	XCDF 289
C * READ REACTION SPECIFICATION CARD AND CONVERT CONSTANTS A AND C	XCDF 290
C * INTO ONE COMBINED CONSTANT A FOR EACH PRESSURE SEPARATELY	XCDF 291
C ***	XCDF 292
520 READ 521,(RENAME(J),J=1,10),A,B,C,CDMOL,WAMOL,JPLOT	XCDF 293
521 FORMAT(10A4,3F8.0,2F6.0,14)	XCDF 294
IF(CDMOL.LT.0.) GO TO 106	XCDF 295
DO 522 N=1,NOPRES	XCDF 296
PTOTAL=IPRES(N)	XCDF 297
ECCDEF(1,N,1)=A+C*(PTOTAL-2000.)	XCDF 298
522 CONTINUE	XCDF 299
KONVRA=A	XCDF 300
DO 104 N=1,NOPRES	XCDF 301
A=ECCDEF(1,N,1)	XCDF 302
NOTA=1	XCDF 303
IPAGE=1	XCDF 304
NP=N+NOPRES	XCDF 305
PTOTAL=IPRES(N)	XCDF 306
PL=PTOTAL*.0005	XCDF 307
SL=PL*.03	XCDF 308
PRINT 53,(RENAME(J),J=1,10),IPRES(N),WORD(3),IPAGE,KONVRA,	XCDF 309
1 8,C	XCDF 310
53 FORMAT(1H1,9H REACTION,10A4,22HAT A TOTAL PRESSURE OF,15,A4,	XCDF 311
1 20X,4HPAGE,12/51X,2HA=,17,4H, 8=,F7.3,4H, C=,F6.4)	XCDF 312
54 FORMAT(1H1,9H REACTION,10A4,22HAT A TOTAL PRESSURE OF,15,A4,	XCDF 313
1 20X,4HPAGE,12/)	XCDF 314
IPAGE=IPAGE+1	XCDF 315
C ***	XCDF 316
C * IF DIAGRAM REQUESTED, INITIALIZE PORTION OF STORAGE ARRAY	XCDF 317
C ***	XCDF 318
IF(JPLOT.GT.0) GO TO 541	XCDF 319
IF(IPLT.EC.0) GO TO 543	XCDF 320
541 DO 542 K=1,83	XCDF 321
DO 542 J=1,3	XCDF 322
IRA(K,N,J)=0	XCDF 323
542 CONTINUE	XCDF 324
C ***	XCDF 325
CONTROLS THE MAIN FLOW ACCORDING TO THE TYPE OF THE REACTION	XCDF 326
C ***	XCDF 327
543 IF(WAMOL)79,780,55	XCDF 328
55 NOTA=2	XCDF 329
IF(CDMOL)106,781,56	XCDF 330
C ***	XCDF 331
C * IF H2O AND CO2 ON SAME SIDE, START TO DETERMINE MAXIMUM TEMPERATURE	XCDF 332
C ***	XCDF 333
56 INDEX=INTVAL	XCDF 334
PCD=CDMOL*PTOTAL/(CDMOL+WAMOL)	XCDF 335
PCDMIN=PCD	XCDF 336
PWA=PTOTAL-PCD	XCDF 337
PWAMIN=PWA	XCDF 338
ITSTEP=512	XCDF 339
LIMIT=9	XCDF 340
IF(IGRADE.GT.256) GO TO 57	XCDF 341
ITSTEP=256	XCDF 342
LIMIT=8	XCDF 343
IF(IGRADE.GT.128) GO TO 57	XCDF 344
ITSTEP=128	XCDF 345
LIMIT=7	XCDF 346
57 ITEMK=KELMIN	XCDF 347
TEMPK=ITEMK	XCDF 348
FCD=PCD*FUCDEF(IGRADE,NP)	XCDF 349
FWA=PWA*FUCDEF(IGRADE,N)	XCDF 350

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ECTEST=FCD**CDMOL*FWA**WANUL
IF(ECTEST.LT.ECONF(TEMPK)) GO TO 102
ITEMK=MAXTEM+273
TEMPK=ITEMK
FCD=PCD*FUCOEF(1,NP)
FWA=PWA*FUCOEF(1,N)
ECTEST=FCD**CDMOL*FWA**WANUL
IF(ECTEST.LT.ECONF(TEMPK)) GO TO 572
PRINT 571,MAXTEM
571 FOR: AT(30HG MAXIMUM TEMPERATURE IS ABOVE,15,
1 19F DEGREES CENTIGRADE,////)
IT=1
GO TO 63
572 ITEMK=MSTART+273
INDEX=0
IT=0
L=0
58 L=L+1
IF(L.GT.LIMIT) GO TO 62
ITSTEP=IABS(ITSTEP)/2
59 ITEMK=ITEMK-ITSTEP
IT=IT+ITSTEP
IF(ITEMK.GE.KELMIN) GO TO 61
60 L=L+1
IF(L.GT.LIMIT) GO TO 62
ITSTEP=-IABS(ITSTEP)/2
GO TO 59
61 TEMPK=ITEMK
FCD=PCD*FUCOEF(IT,NP)
FWA=PWA*FUCOEF(IT,N)
ECTEST=FCD**CDMOL*FWA**WAMOL
EC=ECONF(TEMPK)
IF(ECTEST-EC)58,63,60
62 IF(ECTEST.LE.EC) GO TO 63
ITEMK=ITEMK+1
TEMPK=TEMPK+1.
IT=IT-1
63 ITMAX=ITEMK-273
C ***
C IF DIAGRAM REQUESTED, STORE MAXIMUM TEMPERATURE AND CO2 FRACTION
C IF CURVE MAXIMUM ABOVE PROGRAM MAXIMUM, PROCEDURE IS MODIFIED
C ***
IF(JPLOT.GT.0) GO TO 630
IF(IPLOT.EC.0) GO TO 632
630 J=(IP-ITMAX)/INTVAL
IRA(83,N,1)=ITMAX
IRA(83,N,3)=INTVAL
IF(INDEX)631,631,640
631 IRA(J,N,1)=ITMAX
IRA(J,N,2)=PCD*100./PTOTAL+.5
IRA(J,N,3)=0
IRA(83,N,2)=1
632 IF(INDEX)633,633,640
633 PRINT 64,ITMAX,PCD,PWA,FCD,FWA
64 FORMAT(21HG MAXIMUM TEMPERATURE,15/6H PCO2,F8.2/6H PH2O,F8.2/
1 6H FCO2,F8.2/6H FH2O,F8.2/)
ITEST=ITMAX/INTVAL
ITEST1=ITEST*INTVAL
IF(ITEST.EQ.ITMAX) GO TO 641
INDEX=ITEST1-ITMAX+INTVAL
640 IT=IT-INDEX
ITMAX=ITMAX+INDEX
641 ITSTEP=(ITMAX-MINTEM)/INTVAL
IF(ITSTEP.LT.1) GO TO 107
INDEX=3
NOUSE=0
PRINT 65
65 FORMAT(56HG ----- CARBON-DIOXIDE FLOR GASES -----//XCDF 418
1 15X,56H----- CARBON-DIOXIDE RICH GASES -----//XCDF 419
2 6H TEMP,5X,4HF02,6X,4HFH2O,6X,4HPCO2,6X,4HPH2O,6X,4HXCO2,6X, XCDF 420
3 4HTEMP,8X,4HF02,6X,4HFH2O,6X,4HPCO2,6X,4HPH2O,6X,4HXCO2,6X, XCDF 421
4 4HTEMP/) XCDF 422
LINES=14 XCDF 423
C *** XCDF 424
C * TRACE BOTH BRANCHES OF EQUILIBRIUM CURVE FROM MAXIMUM TEMPERATURE XCDF 425
C * DOWNWARD UNTIL BOTH VALUES OF X-CO2 OUT OF RANGE XCDF 426
C *** XCDF 427
DO 78 I=1,ITSTEP XCDF 428
IF(NOUSE.GT.2) GO TO 104 XCDF 429
ITMAX=ITMAX-INTVAL XCDF 430
TEMPK=ITMAX+273 XCDF 431
IT=IT+INTVAL XCDF 432
66 EC=ECONF(TEMPK) XCDF 433
PCD=PCDMIN*.5 XCDF 434
PSTEP=PCD XCDF 435
GO TO 65 XCDF 436
67 PCD=PCD+PSTEP XCDF 437
GO TO 65 XCDF 438

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68	PCD=PCD-PSTEP	XCDF	439
69	PSTEP=PS1LF*.5	XCDF	440
	PWA=PTOTAL-PCD	XCDF	441
	FWA=PWA*FUCDEF(11,N)	XCDF	442
	FCD=PCD*FUCDEF(11,NP)	XCDF	443
	IF(PSTEP.LT.SL) GO TO 70	XCDF	444
	ECTEST=FCD**CDMOL*FWA**WAMOL	XCDF	445
	IF(ECTEST-EC)67,70,68	XCDF	446
70	PCDMIN=PCD	XCDF	447
	PCDLO=PCD	XCDF	448
	XCDLO=PCD/PTOTAL	XCDF	449
	FCDLO=FCD	XCDF	450
	PWALO=PWA	XCDF	451
	FWALO=FWA	XCDF	452
	IF(NOUSE.EQ.2) GO TO 71	XCDF	453
	IF(PCC.LT.PL) NOUSE=NOUSE+2	XCDF	454
71	PWA=PWAMIN*.5	XCDF	455
	PSTEP=PWA	XCDF	456
	GO TO 74	XCDF	457
72	PWA=PWA+PSTEP	XCDF	458
	GO TO 74	XCDF	459
73	PWA=PWA-PSTEP	XCDF	460
74	PSTEP=PSTEP*.5	XCDF	461
	PCD=PTOTAL-PWA	XCDF	462
	FWA=PWA*FUCDEF(11,N)	XCDF	463
	FCD=PCD*FUCDEF(11,NP)	XCDF	464
	IF(PSTEP.LT.SL) GO TO 75	XCDF	465
	ECTEST=FCD**CDMOL*FWA**WAMOL	XCDF	466
	IF(EC-ECTEST)73,75,72	XCDF	467
75	XCD=PCD/PTOTAL	XCDF	468
	PWAMIN=PWA	XCDF	469
	IF(NOUSE.EQ.1) GO TO 751	XCDF	470
	IF(PWAMIN.LT.PL) NOUSE=NOUSE+1	XCDF	471
751	IF(LINES.LT.LP) GO TO 76	XCDF	472
	PRINT 54,(RENAME(J),J=1,10),IPRES(N),WORD(3),IPAGE	XCDF	473
	PRINT 65	XCDF	474
	LINES=7	XCDF	475
	IPAGE=IPAGE+1	XCDF	476
76	PRINT 77,ITMAX,FCDLO,FWALO,PCDLO,PWALO,XCDLO,ITMAX,FCD,FWA,PCD,PWAX	XCDF	477
	1,XCD,ITMAX	XCDF	478
77	FORMAT(I6,4F10.2,F10.5,3X,I6,3X,4F10.2,F10.5,3X,I6)	XCDF	479
	LINES=LINES+1	XCDF	480
C ***		XCDF	481
C * IF DIAGRAM REQUESTED, STORE TEMPERATURE AND X-CC2 FOR PLOTTING		XCDF	482
C ***		XCDF	483
	IF(JPLOT.GT.0) GO TO 771	XCDF	484
	IF(IPLT.EQ.0) GO TO 78	XCDF	485
771	J=(IP-ITMAX)/INTVAL	XCDF	486
	IF(INDEX.GT.82) GO TO 78	XCDF	487
	IF(INDEX-23)776,772,773	XCDF	488
772	IF(XCDLO.GE..005) GO TO 775	XCDF	489
	INDEX=INDEX+60	XCDF	490
	GO TO 78	XCDF	491
773	IF(XCD.LT..995) GO TO 774	XCDF	492
	INDEX=INDEX+20	XCDF	493
	GO TO 78	XCDF	494
774	IRA(J,N,3)=XCD*100.+5	XCDF	495
	GO TO 779	XCDF	496
775	IRA(J,N,2)=XCDLO*100.+5	XCDF	497
	GO TO 779	XCDF	498
776	IF(XCD.LT..995) GO TO 777	XCDF	499
	INDEX=INDEX+20	XCDF	500
	GO TO 772	XCDF	501
777	IF(XCDLO.GE..005) GO TO 778	XCDF	502
	INDEX=INDEX+60	XCDF	503
	GO TO 774	XCDF	504
778	IRA(J,N,3)=XCD*100.+5	XCDF	505
	IRA(J,N,2)=XCDLO*100.+5	XCDF	506
779	IRA(J,N,1)=ITMAX	XCDF	507
	IRA(83,N,2)=IRA(83,N,2)+1	XCDF	508
	78 CONTINUE	XCDF	509
C ***		XCDF	510
CALCULATIONS DISCONTINUED BECAUSE MINIMUM TEMPERATURE ATTAINED		XCDF	511
C ***		XCDF	512
	GO TO 104	XCDF	513
780	CALL ONEMOB(N,NOPRES, INTVAL,CDMOL,IGRADE,KELMIN,MINTEM,BOTTEM,	XCDF	514
	1 NOTA,A,B,PTOTAL,IP,IPLT,JPLOT,PL,LP)	XCDF	515
	GO TO 104	XCDF	516
781	CALL ONEMOB(N,NOPRES, INTVAL,WAMOL,IGRADE,KELMIN,MINTEM,BUTTEM,	XCDF	517
	1 NOTA,A,B,PTOTAL,IP,IPLT,JPLOT,PL,LP)	XCDF	518
	GO TO 104	XCDF	519
C ***		XCDF	520
CO2 AND H2O ON DIFFERENT SIDES OF CHEMICAL EQUATION		XCDF	521
C ***		XCDF	522
79	PRINT 80	XCDF	523
80	FORMAT(6H0 TEMP,5X,4HXC02,6X,4HPC02,6X,4HFCC2,6X,4HPH20,6X,	XCDF	524
	1 4HFH20/)	XCDF	525
	LINES=5	XCDF	526

NOTA=0	XCDF 527
WMOLE=-WAMOL	XCDF 528
ITEST=MAXTEM/INTVAL	XCDF 529
ITMAX=ITEST*INTVAL+INTVAL	XCDF 530
INDEX=ITMAX-MAXTEM	XCDF 531
IT=1-INDEX	XCDF 532
INDEX=1	XCDF 533
ITSTEP=(ITMAX-MINTEM)/INTVAL	XCDF 534
C ***	XCDF 535
C * DETERMINE WHETHER CURVE SLOPES TO THE LEFT OR TO THE RIGHT	XCDF 536
C ***	XCDF 537
IF(A.LE.0.) GO TO 83	XCDF 538
TEMPK=MAXTEM+273	XCDF 539
ECMIN=ECONF(TEMPK)	XCDF 540
FCD=FUCDEF(1,NP)	XCDF 541
FWA=FUCDEF(1,N)	XCDF 542
ECTMIN=FCD**CDMOL/FWA**WMOLE	XCDF 543
EC=ECONF(601TEM)	XCDF 544
EC=EC/ECMIN	XCDF 545
FCD=FUCDEF(IGRADE,NP)	XCDF 546
FWA=FUCDEF(IGRADE,N)	XCDF 547
ECTEST=FCD**CDMOL/FWA**WMOLE	XCDF 548
ECTEST=ECTEST/ECTMIN	XCDF 549
IF(ECTEST-EC)82,81,83	XCDF 550
C ***	XCDF 551
C * POINTER NOTA IS SET UP TO SIGNAL TYPE OF SLOPE+ NOTA=0 FOR REGULAR	XCDF 552
CASE, NOTA=1 FOR REVERSED SLOPE, NOTA=2 FOR INTERMEDIATE CASE	XCDF 553
C ***	XCDF 554
61 NOTA=NOTA+1	XCDF 555
62 NOTA=NOTA+1	XCDF 556
63 DO 101 I=1,ITSTEP	XCDF 557
PCD=0	XCDF 558
PSTEP=PTOTAL	XCDF 559
IT=IT+INTVAL	XCDF 560
ITMAX=ITMAX-INTVAL	XCDF 561
TEMPK=ITMAX+273	XCDF 562
EC=ECONF(TEMPK)	XCDF 563
64 PSTEP=PSTEP*.5	XCDF 564
IF(PSTEP.LT.SL) GO TO 87	XCDF 565
PCD=PCD+PSTEP	XCDF 566
65 PWA=PTOTAL-PCD	XCDF 567
FCD=PCD*FUCDEF(1,NP)	XCDF 568
FWA=PWA*FUCDEF(IT,N)	XCDF 569
ECTEST=FCD**CDMOL/FWA**WMOLE	XCDF 570
IF(ECTEST-EC)84,87,86	XCDF 571
66 PSTEP=PSTEP*.5	XCDF 572
IF(PSTEP.LT.SL) GO TO 87	XCDF 573
PCD=PCD-PSTEP	XCDF 574
GO TO 85	XCDF 575
87 XCD=PCD/PTOTAL	XCDF 576
IF(NOTA-1)88,90,89	XCDF 577
88 IF(PWA.LT.PL) GO TO 101	XCDF 578
89 IF(LINES.LT.LP) GO TO 91	XCDF 579
PRINT 54,(RENAME(J),J=1,10),IPRES(N),WORD(3),IPAGE	XCDF 580
PRINT 80	XCDF 581
LINES=5	XCDF 582
IPAGE=IPAGE+1	XCDF 583
GO TO 91	XCDF 584
90 IF(PCD-PL)101,89,89	XCDF 585
91 PRINT 92,ITMAX,XCD,PCD,FCD,PWA,FWA	XCDF 586
92 FORMAT(I6,F10.5,4F10.2)	XCDF 587
LINES=LINES+1	XCDF 588
IF(NOTA-1)94,93,95	XCDF 589
93 IF(PWA-1.)104,93,95	XCDF 590
94 IF(PCD.LT.1.) GO TO 104	XCDF 591
C ***	XCDF 592
C * IF DIAGRAM REQUESTED, STORE VALUES TO BE PLOTTED LATER BY IGRAPH	XCDF 593
C ***	XCDF 594
95 IF(JPLOT.GT.0) GO TO 951	XCDF 595
IF(IPLOT.EC.0) GO TO 101	XCDF 596
951 IF(INDEX.GT.82) GO TO 101	XCDF 597
IF(NOTA-1)96,97,99	XCDF 598
96 IF(XCD-.005)100,99,98	XCDF 599
97 IF(>XCD.GE..95) GO TO 100	XCDF 600
IF(XCD-.005)101,99,99	XCDF 601
98 IF(XCD.GE..95) GO TO 101	XCDF 602
99 J=(1P-ITMAX)/INTVAL	XCDF 603
IRA(J,N,1)=ITMAX	XCDF 604
IRA(J,N,2)=XCD*100.+5	XCDF 605
IRA(J,N,3)=0	XCDF 606
IRA(83,N,2)=IRA(83,N,2)+1	XCDF 607
IF(IRA(83,N,2).GT.1) GO TO 101	XCDF 608
IRA(83,N,1)=ITMAX	XCDF 609
IRA(83,N,3)=INTVAL	XCDF 610
GO TO 101	XCDF 611
100 INDEX=83	XCDF 612
101 CONTINUE	XCDF 613
GO TO 104	XCDF 614

102 PRINT 103,MINTEM	XCDF 615
103 FORMAT(52H0 MAXIMUM TEMPERATURE IS BEL(W THE SPECIFIED MINIMUM,	XCDF 616
1 15H TEMPERATURE (OF,14,19H DEGREES CENTIGRADE)	XCDF 617
GO TO 104	XCDF 618
107 ITMAX=ITMAX-INDX	XCDF 619
PRINT 106, IPRES(N),ITMAX	XCDF 620
108 FORMAT(24H OTHER CALCULATIONS FOR,15,20H BAR SKIPPED BECAUSE,	XCDF 621
1 28H MAXIMUM TEMPERATURE IS ONLY,14,19H DEGREES CENTIGRADE)	XCDF 622
104 CONTINUE	XCDF 623
C ***	XCDF 624
CONTROL HAS TO GO TO SUBROUTINE IGRAPH UNDER EITHER PLOTTING OPTION	XCDF 625
C ***	XCDF 626
IF(JPLOT.GT.0) GO TO 105	XCDF 627
IF(1PLOT)105,520,105	XCDF 628
105 CALL IGRAPH(INTVAL,MINTEM,MAXTEM,IP,NOPRES,LP)	XCDF 629
GO TO 520	XCDF 630
106 CALL EXIT	XCDF 631
END	XCDF 632
SUBROUTINE ONEJOB(NC,NOPRES,INTVAL,FLMOL,IGRADE,KELMIN,MINTEM,	XCDF 633
1 BOTTEM,NOTA,A,B,PTOTAL,IP,IPLCT,JPLOT,PL,LP)	XCDF 634
DIMENSION FUCOEF(406,8)	XCDF 635
COMMON FUCOEF	XCDF 636
COMMON/AAA/EQCOEF(2,4,9),WORD(3)	XCDF 637
COMMON/EBB/IPRES(4),RENAME(10),SYMBLL(10),PLINE(101),IRA(83,4,3)	XCDF 638
C ***	XCDF 639
CHEMICAL EQUATION SHOWS ONLY ONE MOBILE COMPONENT	XCDF 640
C ***	XCDF 641
C *** IF THE EXTERNAL-DECLARATION OF XCDFCR 6 IS USED, THE FOLLOWING	XCDF 641
C *** STATEMENT MUST BE REMOVED	XCDF 641
ECONF(TEMPK)=10.**(A/TEMPK+B)	XCDF 641
IPAGE=2	XCDF 642
N=NC	XCDF 643
LINES=5	XCDF 644
IF(NOTA.EG.2) GO TO 2	XCDF 645
NO=NC+NOPRES	XCDF 646
GO TO 4	XCDF 647
1 FORMAT(35H0 TEMP XCO2 PCO2 FCO2/)	XCDF 648
2 NO=NC	XCDF 649
3 FORMAT(35H0 TEMP XH2O PH2O FH2O/)	XCDF 650
4 CMOLE=1./FLMOL	XCDF 651
C ***	XCDF 652
C * BEGIN CALCULATIONS BY DETERMINING MAXIMUM TEMPERATURE	XCDF 653
C ***	XCDF 654
PCD=PTOTAL	XCDF 655
ITSTEP=512	XCDF 656
LIMIT=9	XCDF 657
IF(IGRADE.GT.256) GO TO 5	XCDF 658
ITSTEP=ITSTEP/2	XCDF 659
LIMIT=8	XCDF 660
IF(IGRADE.GT.128) GO TO 5	XCDF 661
ITSTEP=ITSTEP/2	XCDF 662
LIMIT=7	XCDF 663
5 ITEMK=KELMIN	XCDF 664
TEMPK=BOTTEM	XCDF 665
FCD=PCD*FUCOEF(IGRADE,NO)	XCDF 666
ECTEST=FCD*FLMOL	XCDF 667
IF(ECTEST.LT.ECONF(TEMPK)) GO TO 21	XCDF 668
ITEMK=ITEMK+IGRADE	XCDF 669
IT=0	XCDF 670
L=0	XCDF 671
6 L=L+1	XCDF 672
IF(L.GT.LIMIT) GO TO 10	XCDF 673
ITSTEP=IABS(ITSTEP/2)	XCDF 674
7 ITEMK=ITEMK-ITSTEP	XCDF 675
IT=IT+ITSTEP	XCDF 676
IF(ITEMK.LT.KELMIN) GO TO 8	XCDF 677
TEMPK=ITEMK	XCDF 678
FCD=PCD*FUCOEF(IT,NO)	XCDF 679
EC=ECONF(TEMPK)	XCDF 680
ECTEST1=FCD*FLMOL	XCDF 681
IF(ECTEST1-EC)6,10,8	XCDF 682
8 L=L+1	XCDF 683
IF(L.GT.LIMIT) GO TO 10	XCDF 684
ITSTEP=-IABS(ITSTEP/2)	XCDF 685
GO TO 7	XCDF 686
9 TEMPK=TEMPK-1.	XCDF 687
IT=IT+1	XCDF 688
IF(11.GT.IGRADE) GO TO 21	XCDF 689
10 EC=ECONF(TEMPK)	XCDF 690
FCD=EC*CMOLE	XCDF 691
PCD=FCD/FUCOEF(IT,NO)	XCDF 692
IF(PCD.GT.PTOTAL) GO TO 9	XCDF 693
ITMAX=TEMPK-273.	XCDF 694
IF(NOTA.EG.2) GO TO 11	XCDF 695
XCD=PCD/PTOTAL	XCDF 696
GO TO 12	XCDF 697
11 XCD=1.-PCD/PTOTAL	XCDF 698
12 IF(NOTA.EG.2) GO TO 121	XCDF 699

PRINT 1	XCDF 700
GO TO 122	XCDF 701
121 PRINT 3	XCDF 702
122 PRINT 13,ITMAX,XCD,PCD,FCD	XCDF 703
13 FORMAT(I6,F10.5,2F10.2)	XCDF 704
LINES=LINES+1	XCDF 705
C ***	XCDF 706
C * STORE VALUES IF DIAGRAM REQUESTED	XCDF 707
C ***	XCDF 708
INDEX=0	XCDF 709
IF(JPLOT.GT.0) GO TO 131	XCDF 710
IF(IPLOT.EC.0) GO TO 132	XCDF 711
131 J=(IP-ITMAX)/INTVAL	XCDF 712
IRA(J,N,1)=ITMAX	XCDF 713
IRA(J,N,2)=XCD*100.+5	XCDF 714
IF(IRA(J,N,2).LT.1) IRA(J,N,2)=101	XCDF 715
IRA(J,N,3)=0	XCDF 716
IRA(83,N,1)=ITMAX	XCDF 717
IRA(83,N,2)=1	XCDF 718
IRA(83,N,3)=INTVAL	XCDF 719
C ***	XCDF 720
C * PREPARE FOR SCANNING THE CURVE DOWNSLOPE AT INTERVALS SPECIFIED	XCDF 721
C ***	XCDF 722
132 ITEST=ITMAX/INTVAL	XCDF 723
ITEST=ITEST*INTVAL	XCDF 724
IF(ITEST.EQ.ITMAX) GO TO 14	XCDF 725
INDEX=ITEST-ITMAX+INTVAL	XCDF 726
IT=IT-INDEX	XCDF 727
ITMAX=ITMAX+INDEX	XCDF 728
14 ITSTEP=(ITMAX-MINTEM)/INTVAL	XCDF 729
IF(ITSTEP.LT.1) GO TO 221	XCDF 730
INDEX=J	XCDF 731
DO 20 I=1,ITSTEP	XCDF 732
INDEX=INDEX+1	XCDF 733
ITMAX=ITMAX-INTVAL	XCDF 734
TEMPK=ITMAX+273	XCDF 735
IT=IT+INTVAL	XCDF 736
J=J+1	XCDF 737
EC=ECONF(TEMPK)	XCDF 738
FCD=EC*CMOLE	XCDF 739
PCD=FCD/FUCDEF(IT,NO)	XCDF 740
IF(NOTA.EQ.2) GO TO 15	XCDF 741
XCD=PCD/PTOTAL	XCDF 742
GO TO 16	XCDF 743
15 XCD=1.-PCD/PTOTAL	XCDF 744
16 IF(LINES.L1.LP) GO TO 188	XCDF 745
PRINT 17,(RENAME(K),K=1,10),IPRES(N),WORD(3),IPAGE	XCDF 746
17 FORMAT(10H1 REACTION,10A4,4X,22HAT A TOTAL PRESSURE OF,15,A4,	XCDF 747
1 20X,4HPAGE,I2/)	XCDF 748
IF(NOTA.EQ.2) GO TO 18	XCDF 749
PRINT 1	XCDF 750
GO TO 187	XCDF 751
18 PRINT 3	XCDF 752
187 LINES=5	XCDF 753
IPAGE=IPAGE+1	XCDF 754
188 PRINT 13,ITMAX,XCD,PCD,FCD	XCDF 755
LINES=LINES+1	XCDF 756
IF(PCD.LT.PL) GO TO 23	XCDF 757
IF(INDEX.GT.82) GO TO 20	XCDF 758
C ***	XCDF 759
C * STORE VALUES IF DIAGRAM REQUESTED	XCDF 760
C ***	XCDF 761
IF(JPLOT.GT.0) GO TO 191	XCDF 762
IF(IPLOT.EC.0) GO TO 20	XCDF 763
191 IRA(J,N,1)=ITMAX	XCDF 764
IRA(J,N,2)=XCD*100.+5	XCDF 765
IRA(J,N,3)=0	XCDF 766
IRA(83,N,2)=IRA(83,N,2)+1	XCDF 767
IF(NOTA-1)192,193,192	XCDF 768
192 IF(IRA(J,N,2)-100)20,194,194	XCDF 769
193 IF(IRA(J,N,2).GE.1) GO TO 20	XCDF 770
194 IRA(83,N,2)=IRA(83,N,2)-1	XCDF 771
IRA(J,N,1)=0	XCDF 772
IRA(J,N,2)=0	XCDF 773
INDEX=83	XCDF 774
20 CONTINUE	XCDF 775
GO TO 23	XCDF 776
21 PRINT 22,MINTEM	XCDF 777
22 FORMAT(30HC MAXIMUM TEMPERATURE IS BELOW,I4,8H DEGREES ,	XCDF 778
1 10HCENTIGRADE)	XCDF 779
GO TO 23	XCDF 780
221 ITMAX=ITMAX-INDEX	XCDF 781
PRINT 222, IPRES(N),ITMAX	XCDF 782
222 FORMAT(25H FURTHER CALCULATIONS FOR,15,20H BAR SKIPPED BECAUSE,	XCDF 783
1 28H MAXIMUM TEMPERATURE IS ONLY,I4,19H DEGREES CENTIGRADE)	XCDF 784
23 RETURN	XCDF 785
END	XCDF 786
SUBROUTINE JGRAPH(INTVAL,MINTEM,MAXTEM,IP,NUPRES,LP)	XCDF 787

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COMMON/BBB/IPRES(4),RENAME(10),SYMBOL(10),PLINE(101),IRA(83,4,3) XCDF 788
GO TO (40,42,44,46), NOPRES XCDF 789
40 PRINT 41, (RENAME(J),J=1,10), IPRES(1) XCDF 790
41 FORMAT(1H1,15X,27H1/XCO2 DIAGRAM FOR REACTION,10A4,2HAT,15,4H BAR) XCDF 791
C ***** XCDF 792
GO TO 48 XCDF 793
42 PRINT 43, (RENAME(J),J=1,10), (IPRES(J),J=1,2) XCDF 794
43 FORMAT(1H1,10X,27H1/XCO2 DIAGRAM FOR REACTION,10A4,2HAT,15,4H AND, XCDF 795
1 15,4H BAR) XCDF 796
GO TO 44 XCDF 797
44 PRINT 45, (RENAME(J),J=1,10), (IPRES(J),J=1,3) XCDF 798
45 FORMAT(1H1,5X,27H1/XCO2 DIAGRAM FOR REACTION,10A4,2HAT,2(15,1H,), XCDF 799
1 4H AND,15,4H BAR) XCDF 800
GO TO 46 XCDF 801
46 PRINT 47, (RENAME(J),J=1,10), (IPRES(J),J=1,4) XCDF 802
47 FORMAT(28H11/XCO2 DIAGRAM FOR REACTION,10A4,2HAT,3(15,1H,),4H AND, XCDF 803
1 15,4H BAR) XCDF 804
48 MAXTMP=MINTEM XCDF 805
MINTMP=MAXTEM XCDF 806
DO 3 J=1,NOPRES XCDF 807
IF(IRA(83,J,2).EQ.0) GO TO 3 XCDF 808
MINTRY=IRA(83,J,1)-INTVAL*IRA(83,J,2)+INTVAL XCDF 809
IF(MAXTMP.GE.IRA(83,J,1)) GO TO 2 XCDF 810
MAXTMP=IRA(83,J,1) XCDF 811
2 IF(MINTRY.GE.MINTMP) GO TO 3 XCDF 812
MINTMP=MINTRY XCDF 813
3 CONTINUE XCDF 814
IF(MAXTMP.LT.MINTMP) GO TO 20 XCDF 815
ITEST=MAXTMP/INTVAL XCDF 816
ITEST1=ITEST*INTVAL XCDF 817
IF(ITEST.EQ.MAXTMP) GO TO 4 XCDF 818
MLINE=ITEST1+INTVAL XCDF 819
GO TO 5 XCDF 820
4 MLINE=ITEST1 XCDF 821
5 ITEST=MINTMP/INTVAL XCDF 822
ITEST1=ITEST*INTVAL XCDF 823
IF(ITEST.EQ.MINTMP) GO TO 6 XCDF 824
MINTMP=ITEST1+INTVAL XCDF 825
6 NOLIN=(MLINE-MINTMP)/INTVAL XCDF 826
IF(NOLIN.LT.1) GO TO 20 XCDF 827
J=(IP-MAXTMP)/INTVAL XCDF 828
K=J+NOLIN XCDF 829
IPAGE=0 XCDF 830
LPLOT=LP-2 XCDF 831

IF(NOLIN.LT.LPLOT) GO TO 64 XCDF 832
L=J+LPLOT XCDF 833
DO 63 M=1,NOPRES XCDF 834
IF(IRA(L,M,2).GE.10) GO TO 61 XCDF 835
IF(IRA(L,M,3).GE.10) GO TO 62 XCDF 836
GO TO 63 XCDF 837
61 IF(IRA(L,M,2).LE.90) GO TO 65 XCDF 838
IF(IRA(L,M,3).GE.10) GO TO 62 XCDF 839
GO TO 63 XCDF 840
62 IF(IRA(L,M,3).LE.90) GO TO 65 XCDF 841
63 CONTINUE XCDF 842
64 IPAGE=IPAGE+1 XCDF 843
65 IPAGE=IPAGE+1 XCDF 844
LINES=1 XCDF 845
LPLOT=LPLOT-1 XCDF 846
IF(IPAGE.EQ.1) LINES=-1 XCDF 847
MLINE=MLINE+INTVAL XCDF 848
DO 19 L=J,K XCDF 849
MLINE=MLINE-INTVAL XCDF 850
PLINE(1)=SYMBOL(9) XCDF 851
PLINE(101)=SYMBOL(9) XCDF 852
DO 7 M=2,100 XCDF 853
PLINE(M)=SYMBOL(5) XCDF 854
7 CONTINUE XCDF 855
DO 8 M=11,91,10 XCDF 856
PLINE(M)=SYMBOL(10) XCDF 857
8 CONTINUE XCDF 858
DO 10 M=1,NOPRES XCDF 859
IF(IRA(L,M,2).EQ.0) GO TO 9 XCDF 860
IF(IRA(L,M,2).EQ.101) IRA(L,M,2)=0 XCDF 861
NL=IRA(L,M,2)+1 XCDF 862
PLINE(NL)=SYMBOL(M) XCDF 863
9 IF(IRA(L,M,3).EQ.0) GO TO 10 XCDF 864
NL=IRA(L,M,3)+1 XCDF 865
PLINE(NL)=SYMBOL(M) XCDF 866
10 CONTINUE XCDF 867
MARGIN=MLINE-INTVAL XCDF 868
INDEX=1 XCDF 869
DO 11 M=1,NOPRES XCDF 870
NL=IRA(L,M,1) XCDF 871
IF(NL.EQ.0) GO TO 11 XCDF 872
IF(NL.EQ.MLINE) GO TO 11 XCDF 873
IF(NL.GT.MARGIN) MARGIN=NL XCDF 874
INDEX=0 XCDF 875

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11 CONTINUE	XCDF 876
IF(INDEX.EC.0) GO TO 12	XCDF 877
MARGIN=MLINE	XCDF 878
ITEST=MLINE/INTVAL	XCDF 879
ITEST=ITEST/5	XCDF 880
ITEST=ITEST*5*INTVAL	XCDF 881
IF(ITEST.NE.MARGIN) GO TO 16	XCDF 882
12 IF(LINES.LT.LPLOT) GO TO 14	XCDF 883
PRINT 15,MARGIN,(PLINE(I),I=1,101),MARGIN	XCDF 884
121 IF(JPAGE.GT.1) GO TO 22	XCDF 885
PRINT 13	XCDF 886
13 FORMAT(1H1)	XCDF 887
LINES=1	XCDF 888
IPACE=IPAGE+1	XCDF 889
LOLD=L	XCDF 890
L=K-LPLOT+1	XCDF 891
IF(L.GT.LOLD) L=LOLD	XCDF 892
MLINE=MLINE+(LOLD-L)*INTVAL	XCDF 893
GO TO 19	XCDF 894
14 PRINT 15,MARGIN,(PLINE(I),I=1,101),MARGIN	XCDF 895
15 FORMAT(15,1X,101A1,I4)	XCDF 896
LINES=LINES+1	XCDF 897
GO TO 19	XCDF 898
16 IF(LINES.LT.LPLOT) GO TO 18	XCDF 899
PRINT 17,(PLINE(I),I=1,101)	XCDF 900
17 FORMAT(6X,101A1)	XCDF 901
GO TO 121	XCDF 902
18 PRINT 17,(PLINE(I),I=1,101)	XCDF 903
LINES=LINES+1	XCDF 904
19 CONTINUE	XCDF 905
GO TO 22	XCDF 906
20 PRINT 21,MINTEM,*AXTEM	XCDF 907
21 FORMAT(51H CANNOT BE SHOWN BECAUSE THERE ARE NO SUITABLE XCO2,	XCDF 908
1 23H-VALUES IN THE RANGE OF,I4,3H TC,I4,19H DEGREES CENTIGRADE)	XCDF 909
GO TO 27	XCDF 910
22 DO 23 M=2,100	XCDF 911
PLINE(M)=SYMBOL(7)	XCDF 912
23 CONTINUE	XCDF 913
DO 24 M=11,91,10	XCDF 914
PLINE(M)=SYMBOL(9)	XCDF 915
24 CONTINUE	XCDF 916
PRINT 17,(PLINE(I),I=1,101)	XCDF 917
PRINT 25	XCDF 918
25 FORMAT(8H XCO2=.0,7X,3H0.1,7X,3H0.2,7X,3H0.3,7X,3H0.4,7X,3H0.5,	XCDF 919
1 7X,3H0.6,7X,3H0.7,7X,3H0.8,7X,3H0.9,7X,3H1.0)	XCDF 920
DO 26 I=1,4	XCDF 921
DO 26 J=1,3	XCDF 922
IRA(83,I,J)=0	XCDF 923
26 CONTINUE	XCDF 924
27 RETURN	XCDF 925
END	XCDF 926

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